



Answer All Question

Q1: Consider the following two reaction taking place in a batch reactor:



For component A

$$\frac{dCA}{dt} = -k1CACB$$

$$-A \times 13$$

For component B

$$\frac{dCB}{dt} = -k1CACB - k2CBCc$$

$$-A \times 13 - 0.1 A \times C$$

For component C

$$\frac{dCc}{dt} = k1CACB - k2CBCc$$

$$A \times 13 - 0.1 B \times C$$

For component D

$$\frac{dCD}{dt} = k2CBCc$$

$$0.1 B \times C$$

The initial condition is: at $t=0$, $CA=1$ mol/m³, $CB=1$, $CC=0$, and $CD=0$. The rate constant are: $k1=1$ s⁻¹ and $k2=0.1$ s⁻¹. Using the Runge-Kutta fourth order method (matlab), determine the concentration of A, B,C, and D at 10 s.

(25 MARK)

Q2: Using Matlab to Calculate the composition of the liquid and vapour phases for the acetone, acetonitrile, and nitromethane. The feed composition is $Z1=0.25$, $Z2=0.5$, and $Z3=0.25$. At the given temperature: $P1sat =195.75$ kpa, $P2sat=97.84$ kpa, and $P3sat=50.32$ kpa. The pressure of the system is 100 kpa. Assume the system to follow Raoult, s law.

Given:

$$P_i^{sat} = k_i P, \quad y_i = \frac{K_i z_i}{1 - V + V K_i}, \quad x_i = \frac{z_i}{1 - V + V K_i}$$

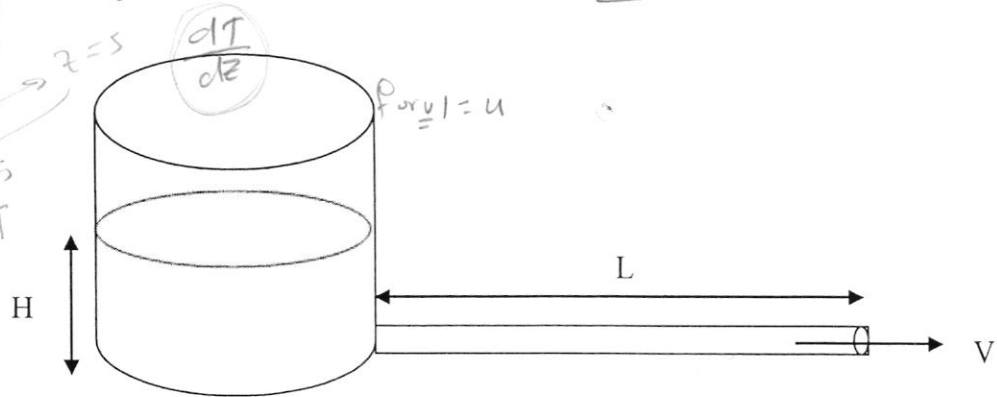
(25 MARK)

Q3: As depicted in fig as show below , the velocity of water, v(m/s), discharged from a cylindrical tank through a long pipe can be computed as

$$v = \sqrt{2gH} \tanh\left(\frac{\sqrt{2gH}}{2L} t\right)$$

Where $g=9.8$ m/s², H =initial head (m), L =pipe length (m), and t =time(s). Determine the head needed to achieve $v=5$ m/s in 2.5 s for 4 m-long pipe (a)graphically (b) by loop-condition.

Handwritten notes: $\sum z = 5$ disp T, $\frac{dT}{dt}$



(25 MARK)

Q4: Consider a binary vapour-liquid equilibrium system. The Antoine equations of the components are given by:

$$\ln P_1 = 16.678 - \frac{3640.2}{T+219.61}$$

where P_1 is saturation pressure.

$$\ln P_2 = 16.2887 - \frac{3816.44}{T+227.02}$$

where P_2 is saturation pressure.

Where the temperature is in C° and the vapour pressure in kpa. The parameters in the Wilson equation are: $a_1=437.98$ and $a_2=1238$. The molar volume of the component is $V_1=76.92 \text{ cm}^3/\text{mol}$ and $V_2=18.07 \text{ cm}^3/\text{mol}$. Assume the system to follow the modified Raoult's. Calculate the bubble point pressure at $100 C^\circ$ and $x_1=0.5$.

The constants are given by:

$$A_1 = V_2/V_1 \exp\left(-\frac{a_1}{RT}\right)$$

$$A_2 = V_1/V_2 \exp\left(\frac{a_2}{RT}\right)$$

The activity coefficients are given by:

$$\ln \beta_1 = -\ln(x_1 + x_2 A_1) + x_2 \left[\frac{A_1}{x_1 + x_2 A_1} - \frac{A_2}{x_2 + x_1 A_2} \right]$$

$$\ln \beta_2 = -\ln(x_2 + x_1 A_2) - x_1 \left[\frac{A_1}{x_1 + x_2 A_1} - \frac{A_2}{x_2 + x_1 A_2} \right]$$

The pressure is given by:

$$P = x_1 \beta_1 P_1 + x_2 \beta_2 P_2$$

(25 MARK)

Good Luck

